JOURNAL OF THE AMERICAN CHEMICAL SOCIETY

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VOLUME 77

SEPTEMBER 27, 1955

Number 18

PHYSICAL AND INORGANIC CHEMISTRY

[Contribution No. 1287 from the Department of Chemistry of Yale University]

The Activity Coefficient of Hydrochloric Acid in Concentrated Aqueous Higher Valence Type Chloride Solutions at 25°. III. The System Hydrochloric Acid-Aluminum Chloride

By Herbert S. Harned and Robert Gary

Received April 1, 1955

The activity coefficient of hydrochloric acid in solutions of aluminum chloride has been determined at 1, 3, 5 total ionic strengths by measurements of the electromotive forces of suitable cells. The rule of the linear variation of the logarithm of the activity coefficient of the acid at constant total ionic strength is closely obeyed. The thermodynamics of the system is developed by the use of the Gibbs-Duhem and cross-differentiation equations.

Electromotive force measurements of cells of the type

$H_2 |HCl(m_1), MCl_3(m_2)|AgCl-Ag$

have been made by Harned and Mason^{1,2} and Mason and Kellam³ on systems containing aluminum and cerium chlorides, respectively. Following the procedure adopted by us⁴ in studying the cells containing barium and strontium chlorides, a precise and extensive series of results have been obtained which form the basis for a thorough exposition of the thermodynamics of the system hydrochloric acid–aluminum chloride–water at high ionic strengths.

Experimental Data.—Table I contains the observed electromotive forces of the cells designated. Each result is the mean of three measurements which agreed to within 0.05 mv.

Activity Coefficients and the Linear Variation of their Logarithms at 1, 3, 5 Constant Ionic Strengths. —Table II contains the activity coefficients of hydrochloric acid computed by the equation

$$E = E^{\circ} - 0.1183 \log \sqrt{\gamma_1^2 m_1 (m_1 + 3m_2)}$$
(1)

As in our earlier calculations,⁴ the value of 0.22246 absolute volt for E° was used. The molalities of the acid and salt are represented by m_1 and m_2 , respectively. The numerical equations given at the top

 H. S. Harned and C. M. Mason, THIS JOURNAL, 53, 3377 (1931).
 H. S. Harned and B. B. Owen, "The Physical Chemistry of Electrolytic Solutions," Reinhold Publ. Corp., New York, N. Y., 1950, p. 458.

(3) C. M. Mason and D. B. Kellam, J. Phys. Chem., 38, 689 (1934).

(4) H. S. Harned and R. Gary, THIS JOURNAL, 76, 5924 (1954); 77, 1994 (1955).

TABLE I

Electromotive Forces in Absolute Volts of the Cells: H₂ (1 Atm.) | HCl ($\mu_1 = m_1$), AlCl₃ (μ_2) | AgCl-Ag at 25° at 1, 3, 5 Total Ionic Strengths

$\mu = 1$		μ	= 3	$\mu = 5$		
m_1	E	m_1	E	m_1	E	
1.0	0.23322	3.0	0.15813	5.0	0.09519	
0.9	. 23799	2.7	. 15841	4.5	. 10290	
.8	. 24321	2 . 4	. 16484	4.0	. 11108	
.7	.24869	2.1	. 17183	3.5	.11968	
.6	.25499	1.8	.17959	3.0	.12897	
. 5	.26207	1.5	.18810	2.5	.13901	
.4	.27024	1.2	. 19794	2.0	. 15036	
.3	.28039	0.9		1.5	. 16334	
. 2	.29349	0.6	.22429	1.0	. 17988	
. 1	.31433	0.3	.24688	0.5	.20383	

of the table were used to test the validity of the linear variation rule. Since 0.1% in γ_1 correspond to about 0.05 mv., the magnitudes of the deviations, $\Delta \gamma_1$, indicate that the linear equations represent the observed results within narrow limits. A possible exception occurs with the results at 5 total ionic strength and low acid concentration where the observed results seem to fall below the calculated ones. At 1 μ the formula used by Harned and Mason¹ was: $\log \gamma_1 = -0.0900 - 0.0605 \,\mu$ which agrees closely with the equation employed by us.

Thermodynamic Considerations.—Following the procedure adopted in our earlier communications,⁴ the assumption is made that the linear variation rule holds within narrow limits for the activity co-

	OBSI	ERVED AND CAL	CULATED A	CHVITY COEF	FICIENTS OF HY	DROCHLORI	C ACID	
		$\Delta \gamma_1 = \gamma_1 (\mathbf{c}$	$(bs.) - \gamma_1$	(calcd.)				
		Eq. used fo	$\mathbf{r} \text{ calen.} \begin{cases} \mu \\ \mu \\ \mu \end{cases}$	= 1; $\log \gamma_1$ = = 3; $\log \gamma_1$ = = 5; $\log \gamma_1$ =	= -0.09091 - 0.11915 - 0.37676 - 0.37676 - 0.0000000000000000000000000000000000	$\begin{array}{c} 0.0614 \ \mu_2 \\ .0629 \ \mu_2 \\ .0631 \ \mu_2 \end{array}$		
				$\mu = 3$			$\mu = 5$	
m_1	γ_1	$\Delta \gamma_1$	m_1	γ' 1	$\Delta \gamma_1$	m_1	γ1	$\Delta \gamma_1$
1.0	0.8111	-0.0003	3.0	1.318	+0.002	5 .0	2.380	-0.001
0.9	.7994	. 0000	2.7	1.254	006	4.5	2.216	+.002
.8	.7870	0012	2.4	1.205	001	4.0	2.059	.000
.7	.7781	+ .0010	2.1	1.157	+ .002	3.5	1.916	+ .002
. 6	.7664	+ .0002	1.8	1,108	+ .002	3.0	1.780	.000
.5	.7555	.0000	1.5	1.062	+ .003	2.5	1.657	+ .002
.4	.7458	+ .0009	1.2	1.015	+ .001	2.0	1.537	002
.3	.7335	0009	0.9			1.5	1.431	.000
.2	.7246	+ .0005	. 6	0.9286	0008	1.0	1.322	009
.1	.7135	0003	. 3	.8872	0026	0.5	1.225	013

 TABLE II

 Observed and Calculated Activity Coefficients of Hydrochloric Acid

efficients of both electrolytic components. Thus

$$\log \gamma_1 = \log \gamma_{1(0)} - \alpha_{12}\mu_2$$
 (2)

$$\log \gamma_2 = \log \gamma_{2(0)} - \alpha_{21}\mu_1$$
(3)
$$\mu = \mu_1 + \mu_2$$
(4)

In these expressions $\gamma_{1(0)}$, $\gamma_{2(0)}$ are the activity coefficients of the acid and salt in water, γ_1 , γ_2 their activity coefficients in the mixtures, μ_1 and μ_2 , their concentrations expressed as ionic strengths and α_{12} and α_{21} are constants at each total ion strength.

If the constant α_{12} is known and equations 2 and 3 are valid, then α_{21} may be computed by the equation

$$\frac{\alpha_{21}}{z_{2+}z_{2-}} = \frac{\alpha_{12}}{z_{1+}z_{1-}} - \frac{2}{2.3 \,\mu} \left[\left(\frac{\phi_1}{z_{1+}z_{1-}} - \frac{\phi_2}{z_{2+}z_{2-}} \right) - \left(\frac{1}{z_{1+}z_{1-}} - \frac{1}{z_{2+}z_{2-}} \right) \right]$$
(5)

where z_{1+} , z_{1-} , z_{2+} , z_2^- are the valences of the ions and ϕ_1 and ϕ_2 are the osmotic coefficients of the two electrolytes in the pure solvent. If the subscripts one and two represent hydrochloric acid and aluminum chloride, respectively, then $z_{2+} = 3$, $z_{2-} =$ $z_{1+} = z_{1-} = 1$ and this equation reduces to

$$\frac{\alpha_{21}}{3} = \alpha_{12} - \frac{0.868}{\mu} \left(\phi_1 - \frac{\phi_2}{3} - 0.667 \right)$$
(6)

From the knowledge of α_{12} and α_{21} , the osmotic coefficient, ϕ_x , in the mixture may be computed by the equation

$$\begin{pmatrix} \frac{\nu_1}{j} \alpha_{12} + \frac{\nu_2}{k} \alpha_{21} \end{pmatrix} \frac{x^2}{2} + \left(\frac{\nu_1}{2.3 \, j\mu} - \frac{\nu_2}{2.3 \, k\mu} - \frac{\nu_2}{k} \alpha_{21} \right) x = \\ \frac{2}{2.3 \, \mu} \frac{\phi_2}{z_{1+} z_{2-}} + \frac{2\phi_x}{2.3 \, \mu} \left(\frac{x}{z_{1+} z_{1-}} + \frac{(1-x)}{z_{2+} z_{2-}} \right)$$
(7)

where ν_1 and ν_2 are the number of ions into which the electrolytes dissociate and the valence factors j and k are defined by the relations $\mu_1 = jm_1, \mu_2 = km_2$. The activity of water and subsequently the water vapor pressure can be obtained by the equation

$$\log a_{w(x)} = \frac{2 \mu \phi_x}{(2.3)5b.5)} \left(\frac{x}{z_{1+} z_{1-}} + \frac{(1-x)}{z_{2+} z_{2-}} \right) \quad (8)^5$$

Table III contains the measured values of α_{12} and values of α_{21} calculated by equation 6. The osmotic coefficients, ϕ_1 and ϕ_2 , were obtained from plots

(5) A typographical error in sign occurs in these last two equations as printed in our earlier communication (ref. 4). The minus sign should be plus in the right hand parentheses in both these equations. This error does not affect any of the calculations. of the data of Stokes⁶ and Robinson and Stokes.⁷ In the second part of the table, similar quantities for the system hydrochloric acid–cerium chloride–water obtained from the data of Mason and Kellam³ are recorded. The values of α_{12} for the cerium chloride mixtures were obtained from measurements of the activity coefficient of the acid at 0.01 M in the cerium chloride solutions and, consequently, are not the result of as comprehensive a study as the present one.

TABLE III

DATA EMPLOYED IN EQUATIONS

					S=
	φ1	φ2	a 12	<i>a</i> 21	$12a_{12} + 4a_{21}$
		(1)	HCl-Al	$Cl_3 - H_2O^8$	
$\mu = 1$	1.039	0.831	0.0614	-0.0636	0.482
$\mu = 2$	1.118	0.905	.062	099	.348
$\mu = 3$	1.348	1.007	.0629	1113	.310
$\mu = 5$	1.680	1.272	.0631	1179	. 286
		(2)	HCl-Ce	Cl ₃ –H ₂ O	
$\mu = 1$	1.039	0.795	0.0870	0177	0.973
$\mu = 2$	1.188	. 847	.0908	0426	.919
$\mu = 3$	1.348	.914	.0918	0510	.898

We have shown that equation 2 expresses within narrow limits the variation of the logarithm of activity coefficient of hydrochloric acid at constant total ionic strength. Since no experimental method is available for determining the activity coefficient of aluminum chloride in these mixtures, we have assumed that its variation is expressed by equation 3. Following a procedure suggested by Glueckauf⁹ which involves fundamental cross differentiation equations, we have shown that, if both equations 2 and 3 are valid, the quantity $S = \nu_1 k \alpha_{12} + \nu_2 j \alpha_{21}$ must be a constant, independent of the total ionic strength, μ . For systems containing a uniunivalent and a triunivalent electrolyte, $S = 12\alpha_{12} + 4\alpha_{21}$. Values of S are recorded in the last column of Table III.

The behavior of S for these acid-triunivalent salt mixtures follows the pattern found for the acid-bi-

(6) R. H. Stokes, Trans. Faraday Soc., 44, 295 (1948).

(7) R. A. Robinson and R. H. Stokes, ibid., 45, 612 (1949).

(8) The result at 2μ was computed from the data of Harned and Mason (reference 1).

(9) E. Glueckauf, H. A. C. McKay and A. R. Mathieson, J. Chem. Soc. S. 299 (1949); Trans. Faraday Soc., 47, 428 (1931).

univalent chloride systems. S appears to decrease rapidly in the more dilute solutions and to approach constancy at the higher concentrations. When the sensitivity of this test is taken into account, it appears that equations 2 and 3 yield a close approximation to the actual behaviors of these mixtures.

For purposes of future comparison, we record in Table IV the hypothetical osmotic coefficients of

TABLE]	[V]
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OSMOTIC COEFFICIENTS AND VAPOR PRESSURES AT 25° OF THE SYSTEM HCl-AlCl₃-H₂O

μ = 1				μ = 3			μ = 5		
m	φx	Þ	m_1	φx	Þ	m_1	φx	Þ	
1.0	1.039	22.88	3.0	1.348	20.54	5.0	1.680	17.55	
0.9	1.026	22.96	2.7	1.327	20.79	4.5	1.651	18.00	
.8	1.013	23.02	2.4	1.306	21.03	4.0	1.622	18.44	
.7	1.000	23.09	2.1	1.282	21.27	3.6	1.592	18.89	
. 6	0.985	23.15	1.8	1.257	21.51	3.0	1.560	19.33	
. 5	.968	23.22	1.5	1.230	21.75	2.5	1.526	19.78	
.4	.950	23.28	1.2	1.199	21.99	2.0	1.488	20.23	
. 3	. 929	23.34	0.9	1.164	22.22	1.5	1.447	20.67	
.2	.904	23.48	.6	1.123	22.46	1.0	1.399	21.12	
. 1	.872	23.49	. 3	1.072	22.69	0.5	1.343	21.57	
.0	. 831	23.52	. 0	1.006	22.91	0.1	1.272	22.01	

the mixtures and the water vapor pressure of the solutions as calculated by equations 7 and 8.

Conclusions

(1) Equation 2 represents within narrow limits the variation of the logarithm of the activity coefficient of hydrochloric acid in aluminum chloride solutions. The values of α_{12} change little with ionic strength in these solutions. A like behavior is found for hydrochloric acid-cerium chloride-water systems.

(2) The calculated values of the quantity α_{21} , vary with ionic strength, and consequently S = $12\alpha_{12} + 4\alpha_{21}$ is found to decrease with increasing concentration. The magnitude of this decrease indicates that in these concentrated solutions, small deviations from results calculated by equation 3 will occur.

This contribution was supported in part by the Atomic Energy Commission under Contract AT-(30-1)1375.

NEW HAVEN, CONN.

[CONTRIBUTION FROM NOVES LABORATORY, DEPARTMENT OF CHEMISTRY AND CHEMICAL ENGINEERING, UNIVERSITY OF ILLINOIS]

Mechanism of Complex Electrode Reactions

By K. B. Oldham

Received February 21, 1955

Several possible mechanisms may be envisaged to explain any complex electrode reaction. By assuming a single step to be rate determining, any postulated mechanism may be reduced to an "equivalent reaction pair," which embodies all the kinetic properties of the mechanism. Account is taken of concentration polarization by including transport processes in the treatment. The procedure is easily extended to cover cases of mixed rate determination. From the equivalent re-action pair, current-voltage relationships can be derived in which it is possible to recognize regions of specific control. The converse operation, the determination of the reaction mechanism from current-voltage curves, is subject to severe limita-tion. The most direct method, examination of the reaction of specific control is applied by for intermediate values of tion. The most direct method, examination of the regions of specific control, is applicable only for intermediate values of the rate constant. Under favorable conditions, experimental data will enable the equivalent reaction pair to be constructed, from which possible mechanisms may be inferred. Mechanisms yielding the same equivalent pair are kinetically indistinguishable.

Analysis of conditions at an electrode surface is greatly simplified if one variable, time, can be ig-nored; hence steady-state conditions only will be treated here. A steady-state electrode system is one in which the activities of all substances present, both at the electrode surface and in the bulk, do not vary appreciably with time, at any potential within the experimental range. Constancy of current is a necessary, though not a sufficient, criterion of steady-state conditions.

The term "electrode reaction" will here denote those processes intimately concerned in the transfer of electrons between an electrode and substances in solution. An electrode reaction may thus involve, in addition to the actual electron transfer, many other reactions, all occurring within a few molecular diameters of the electrode surface. It is convenient to consider the volume in which electrode reactions occur as a zone in which concentrations are uniform and to refer to the activities of substances in this reaction zone as activities "at" the electrode surface. It must be borne in mind that the reaction zone is also occupied by the electrical double layer, but no further mention will be made of this layer on the assumption that any effect of it will be nullified by an excess of indifferent electrolyte, the presence of which will be assumed throughout.

Reaction Rates

Any electrode reaction can be represented by a pair of opposed reactions

over-all reactants + $Ne^- \longrightarrow$ over-all products (1)

expressing the over-all stoichiometry of the reaction. Only for very simple electrode reactions, such as $TI^+ + e^- \rightleftharpoons TI$, however, can it be hoped that (1) will depict the mechanism of the process. For a more complex reaction the most likely mechanism is a sequence of a number, say m, of pairs of opposed reactions

initial reactants initial products (2:1) second reactants reactants (2:2) penultimate reactants penultimate products

$$(2:m-1)$$
final reactants \checkmark final products $(2:m)$

all proceeding at the electrode surface. The possibility of parallel reaction paths is considered in an